# A review of single-phase pressure drop characteristics microchannels with bends

By Endo Junianto

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Endro Junianto a, \*, Jooned Hendrarsakti b

#### Abstract

Microfluidic use in various innovative research, many fields aimed at developing an application device related to handling fluid flows in miniature scale systems. On the other hand, on the use of micro-devices for fluid flow the existence of bends cannot be avoided. This research aims to make a comprehensive study of fluid flow characteristics through a microchannel with several possible bends. This study was conducted by comparing Reynolds number versus pressure drop in a serpentine microchannel to gain bends loss coefficient. The result showed that the fluid flow with Re < 100 did not affect the pressure drop, but on the Reynolds number above that, the pressure drop was increased along with the appears of vortices in the outer and inner walls around the channel bends which causes an increase in an additional pressure drop. The other finding shows that the reduction in diameter bend tube can increase the pressure drop.

Keywords: pressure drop; bend loss coefficient; single-phase; microchannel bends.



# I. Introduction

In recent years, microfluidic tracts have been considerably used in various fields of both engineering and non-engineering. The utilization has also been done as in the heat exchanger for computer CPU coolers [1], fuel cell generators [2][3], micro-mixing reactors [4][5], etc. Regardless of its utilization, the microfluidic system cannot avoid the existence of channel bends which h45 either negative or positive effects. Therefore, it is considered necessary to study the characteristics the fluid flow in a miter bend microchannel. Fluid flows in microchannels are analyzed using the Navier-Stokes equations [6][7] and Direct Simulation Monte Carlo [8][9]. This study was conducted by comparing Reynolds number versus pressure drop in a serpentine microchannel with 900 bend and 1800 bends to obtain the bends loss coefficient. Another microscale effect observation showed that geometry variations of a channel in bends can cause significant additional pressure drop on the fluid flow [10][11]. This work showed that the follow with a low Reynolds number does not affect the pressure drop. Bu 81t the high Reynolds number, the pressure drop increases with the occurrence of vortices in the 51er and inner walls around the channel bends causes an increase in the additional pressure drop [113 Whereas at Re above 1000 the bend loss coefficient Kb almost remains constant and change in the range of ±10 %. The other finding shows that a reduction in diameter bend tube can increase the pressure drop [13][14]. Papautsky

[15] presents experimental findings in the domain of singlephase internal fluid flow at the microscale [16].

This review paper investigates experimental data currently available and assesses the current state-of-the-art. Because the majority of microfluidic bends studies conducted on fluid flows in the laminar regime therefore pressure drop constraints, only laminar data are presented here. Furthermore, a small amount of turbulent data is available for the associated pressure drops.

### II. Materials and Methods

Surface roughness and friction factors have been affected the characteristic of fluid flow in a channel including in the microchannel. Therefore, this section will solvide a brief understanding before mainly discuss about pressure drop, and fluid flow characteristics in the microchannel with bends.

# A. Surface roughness

Kandlikar et al. [17] conducted an expetipental investigation on the surface roughness effect in stainless steel microtube with an inner diameter of 620 μm and 357 μm at Reynolds number range of 500 to 3000. They reported that the surface roughness greatly influences the value of heat transfer and pressure drop. Xing et al. [18] performed studies to see how surface roughness affects flow characteristics in 44 circular microchannels by 10 mm in length and a diameter of 400 μm for Reynolds number

ranges through 150 to 2800. The essential Reynolds number for a conduit with an inner diameter of 400 m was calculated to be around 1500, and the friction factor effect was incressed during the surface roughness escalation. Toghraie et al. [19] investigated the effect of surface roughness to pressure drop in a triangle, rectangular, and trapezoidal cross-section microchannel with number roughness of 3, 6 in the Reynolds number of 5, 10, 15, and 20. They concluded that escalating roughness number would escalate the 32 ressure drop in consequence stagnation effect. Jafari et al. [20] experimentally investigated the effect of the surface roughness of rectangular microchannel evapo 53 r with 700 μm height, and 250 µm width using R134a as the working fluid. They demonstrate that, as the price roughness increase from 2.03 μm - 15.86 μm, the heat transfer coefficient was increased up to 45 %.

Some studies conducted a 23 ulation, as, Guo et al. [21] which numerically modeled the effect of roughness on the fluid flow in the microchannel under laminar flow. They were studied with 2D and 3D Gauss's model where, the 2D model fails to express effect roughness and 3D model is presented sensitively face morphology for both heat transfer and flow resistance. Valde's et al. [22][23] studiens numerical simulation and CFD simulation on the effect of the influence of surface roughness on laminar fluid flow in an annular microchannel. 24 daghiani and Kosar [24] investigated numerically an effect of pin fin shape and surface roughness on heat transfer and gas flow in a rough microchannel. They reported that roughness elements causing Nusselt number decline and pressure drop increase, 57well as surface roughness reduces pin fin shape effect. Lu et al. [25] studied numerically the effect of 2 % roughness in wall square, wave, and limped microchannel with Reynolds number of 500. They showed pressure drop and Nusselt number increase, which also affects the roughness depending on the microchannel's physical shape.

Hydraulic diameter for rectangular cross-section channels determined with:

$$d_h = \frac{4ab}{2(a+b)} \tag{1}$$

Canal aspect ratio,  $\alpha$  is determined as:

$$\alpha = \frac{a}{b} \tag{2}$$

1 When the term "laminar theory" is used to describe a common observation of differences.

$$C^* = \frac{(f \text{ Re})_{experimental}}{(f \text{ Re})_{theoretical}}$$
(3)

Where fRe denotes the non-dimensionalized representation that experimentally and theoretically projected depending on the cross-section for laminar flow First point.

## B. Friction factor

10 Judy et al. [26] performed several experiments with pressure-driven liquid in a round and squa 10 icrochannel of diameter 15 -150 µm with materials of fused silica and stainless steel using distilled water, methanol, and isopropanol for working fluid in the Reynolds number range 8 to 2300. They concluded that the experimental

uncertainty occurred when non-Stokes phenomena were within the diameter ranges. Wu ar 14 chang [27] experimented to measure friction factor laminar flow in trapezoidal smooth silicon microchannel with a hydraulic diameter of 25.9 to 291 µm usi 50 deionized water for working fluid. They suggested that Navier-Stokes equations are app 58 riate for deionized liquid flow in microchannel. Morini et al. [28] conducted an analytical investigation of 18 faction influence on pressure drop incompressible fluid flow in silicon rectangular, trapezoidal, and doubletrapezoidal microchannels. T5 y reported that on condition Mach number under 0.3 the effect of gas rarefaction can separated from compressibility effect and the behavior of the coefficient α vs a function of the 48 rochannel aspect ratio y for the three cross-sections. Silverio and Moreira [29] measured the pressure drop and pressure distribution in cires and square microchannels made of borosilicate glass with hydraulic diameter from 50 to 500 46 in the Reynolds number range from 10 to 2500. Zing Li et al. [30] conducted a computation and experimental investigation on friction factor of gas flow in 11 crochannel with a diameter from 146.7 - 203 µm. They concluded that friction factor and Reynolds number are not in accordance with Moody chart when Mach number is not more than 0.3. Hong et al. [31] studied experimental in friction factor turbulent stream gas in rectangular microchannel made silicon and capped glass with a hydraul 28 ameter of 99.36 and 146.76 µm. They declared that the friction factor could be expressed with a Blasius correlation and Mach number

In the entrance section, the friction factor,  $f_{\rm exp}$  was decided using the pressure difference as follows:

$$f_{\rm exp} = \frac{2_{30}D_h}{\rho V^2}$$
 (4)

12  ${}_{\text{ere}} \Delta P$  is the pressure difference, L is the length device, and V is the mean velocity determined from the mass flow rate.

The theoretical Poiseuille number, Po = f Re, is constant for laminar flow and is a function of  $\alpha$  for rectangular cross-section of 23 els.

Shen et a 27 ] experimental investigation of deionized water flow in 26 rectangular microchannels with a width of 300 µm and a depth of 800 µm, it flowed in the Reynolds number rangeing from 162 to 1257 and temperatures inlet of 30, 50, and 70 °C. They declared that higher inlet deionized water temperat 63 can give better relatively flow performance, and 49 vn that the predicted friction factor value was high 11 when the Reynolds number is low. In order to define friction factor flow in microchannels, Celata 11 /. [35] investigated viscous heating. They expressed that microchannels with a diameter below 100 μm using pressure measurements and evaluation viscous heating be validated friction factor. Gunnasegaran et al. [36] perically studied on laminar flow of water in a triangle, angular, and trapezoidal cross-section microchannel in the 100–1000 29 molds number range. On the rectangular channel, the friction factor and Reynolds number effect appear to 61 rge, according to them. Park and Punch [37] conduced an experimental investigation on friction factor in the rectangular microchannels with hydraulic diameters ranging from 106 to 1/2 μm in the Reynolds number range of 69 - 800. They concluded that the experiment friction factor accord with conventional hydraulic theory, but the heat transfer experimental deviated with Nusselt number

from conventional theory.

43 et al. [38] tested friction factors in a triangular and rectangular microchannel with hydraulic diameters of 400 and 600 m, respectively, using R12 and R134a as working fluids. It is worth noting that the friction factor of both fluids is the same in laminar flow and R12 higher in the turbulent flow.

## III. Result and Discussion

#### A. Pressure Drop

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Pfund et al. [39] measured friction and pressure drop in a rec 64gular microchannel with a depth range from 128 to 521 µm in range of 60 - 3450 Reynolds numbers. They showed that the Reynolds number decreases with decreasing microchannel depth. Bahrami et al. [40] studied the predispose of wall degreeness incompressible laminar flow in a coarse circular microchannel. They reported that the effect of roughness increases the pressure drop but that below 3 % can be neglected. Hwang and Kim [41] investigated on the pressure drop in circular stainless steel microchannel with an inner diameter of 244, 430, and 792 μm when the working fluid is R-134a and the Reynolds number is less than 1000. They make an impression that the first of the flow transition showed a little less than 2300, but on two-phase flow increased the pressure drop with decreasing inner diameter and increasing quality and mass flux. Bahrami et al. [40] co 16 cted some experimentally and numerically analysis on pressure drop of laminar flow in a smooth microchannel with an arbitrary cross-section. They showed that pressure drop from modeling is relatively the same with a numerical analytic result at only an 8 % difference. Q 124 al. [42] conducted computational and experimental studies on the water flow and pressure drop in the rectangular microchannel with 222 μm of width, 694

μm of depth and 120 mm with range of Reynolds numbers from 196 – 2215. They show that the suitability 16 computational and experimental results also proved the conventional Navier-Stokes equation available to predict liquid flow in micro-cooling heat sinks. Hrnjak and Tu [43] studied an investigation on flui 5 and steam flow in the rectangular microchannel with hydraulic diameter from 69,5 to 304,7 μm in the Reynolds number range of 112 – 9180 using R 134a liquid and steam for working fluid. They concluded that both flow in laminar suitable with the analytical solution but on turbulent flow the friction factor higher than analytical solution.

Steinke and Kandlikar [44] determine factor of friction using the fully established flow and Hagenbach factor, as:

$$\Delta \rho = \frac{2(f_{\rm Rc}) \mu \overline{V} L}{D_h^2} + \frac{\kappa(x) \rho \overline{V}^2}{2}$$
 (5)

Where κ is the Hagenbach factor, determined by:

$$\kappa(x) = (f_{app} - f_{FD}) \frac{4x}{D_b} \tag{6}$$

Where  $f_{\rm FD}$  is a fully developed friction factor, then total pressure drop component determines, as:

$$\Delta \rho = \frac{\rho \overline{V}^2}{2} \left[ k_i + k_o + \frac{f_{app} L}{D} \right] \tag{7}$$

The intake loss coefficient is  $k_i$ , while the output loss coefficient is  $k_o$ , then eq. (5) and (7) can be combined, as:

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Author	Year	Fluid/ Form	Form	<u>D<sub>h</sub></u> (μm)	α≈ a/b	Re	C+	f. Re	L/D <sub>h</sub>	Remarks 36
Pfund <i>et al</i> . [39]	2000	Water/ Liquid	R	253- 990	19.19- 78.13	55.3- 3501	0.01- 1.81	0.01- 1.81	101- 396	The essential keynolds number decreases as channel depth decreases. In microchannels, the transition is abrupt but not abrupt.
Judy et al. [26]	2002	Water, methanol, isopropyl	C,R	14- 149	1.00	7.6- 2251	0.83- 1.27	0.83- 1.27	1203- 5657	For 56 ngular channels, pedictions of friction factors are in good agreement with established theories. The material used to construct the microchannel and the test fluid have an impact on the friction factor.
Wu and Cheng [27]	2003	Water/ Liquid	Т	169	1.54- 26.20	16- 1378	0.58- 1.88	0.58- 1.88	192- 467	1
Shen <i>et al</i> . [34]	2006	Water/ Liquid	R	436	2.67	162- 1257	1- 2.84		16-754	In rough microchannels, surface roughness has a 47 antial influence on laminar flow. The value of f Re is greater than what the standard theory predicts for high Reynolds number values, and it grows with increasing Re.
Steinke <i>et al</i> . [44]	2006	Water/ Liquid	R	227	0.8	14- 789	1.15- 3.75		45	The channel cross-section measurements account for the majority of the uncertainty in f. Re.
Hrnjak and Tu [43]	2007	R134a/ Liquid	R	69.5- 304	0.09- 0.24	112- 9180	1.02- 1.09		315- 691	In microch 17 ls, surface roughness raises the friction factor and impacts the transition from laminar to turbulent flow.
Yuan <i>et al</i> . [18]	2016	Water/ liquid	С	400		150- 2800	-	-	25	The friction factor increase when surface roughness increased
Jafari et al.	2016	R134a	R	368	2.8	15.8- 36.8		-	52	Heat transfer experiment increase 45%

circular; R rectangular; Ttrapezoid

$$\Delta \rho_{tot} = \frac{k_i \rho \bar{V}^2}{2} + \frac{k_o \rho \bar{V}^2}{2} + \frac{2(f_{Re}) \mu \bar{V}L}{D_e^2} + \frac{k(x) \rho \bar{V}^2}{2}$$
(8)

Ngo et al. [62] 5] conducted computational and experimental on pressure drop in the microchannel heat exchanger with an S-shaped [54] Fuerstman et al. [46] experimented on pressure drop in a long microchannel with a rectangular cross-section using water and mixtur 7 water and glycerol for working fluid. They concluded that the main contributor per unit length to the pressure drop along of microchannel that loads bubbles is dependent on the concentration of surfactant in the liquid in which the bubbles move.

#### B. Heat transfer

On the channel inner surface with steady heat flux, the border circumstance has a Nusselt number of 4,364 completely developed laminar flo 21

Zhang et al. [47] conduct a study on liquid flow and heat transfer in the rough microchannel. Klein et al. [48] analyzed water flow with alkyl polyglycoside surfactant APG in 26 triangular parallel micro canals with a diameter of 108 μm to gained prime solvent c41centration and mass flux for increasing heat transfer. Lee et al. [49] conducted experimental and numerical on deionized water in the copper rectangular microchannel with hydraulic diameter from 323 - 1068 µm in Reynolds number range of 520 3500 to obtain predicted heat transfer applications in the microchannel. They showed that experimental data accord with the numerical result, but mismatch with the conventional channel correlations i et al. [50] studied numerical and experimental flow and heat transfer characteristic of deionize19 water in microchannel made from silica and stainless with a hydraulic diameter of 50-1570  $\mu m$  in the Reynolds number range from 20 to 2400. They showed that in the hydraulic diameter < 50 µm silica channel the water flower ehavior agrees with macro-scale channel and increases of the Reynolds number affected the heat transfer. Lee and Gapphella [51] presented a research project of saturated flow pressure drop of dejonized water in the silicon rectangular microchannel with a hydraulic diameter range from 162 to 571 µm. They presented the effect of pressure drop. Dai et al. [52] researched the hydrogamic flow through a tortuous microgroove with a semi-circular cross-section in the range of 50 to 900 Reynolds numbers. They concluded that flow in zig-zag

microchannel configuration increased heat transfer rate of effect geometrical parameter. Xu et al. [1] reported they experimentally and numerically study on micro air cooler U–shape for a CPU cooler with rectangular pin fin which has high thermal conductivity and decreases air flow rate.

# C. Flow structure and pressure drop in miter bend microchannel

Taassob et al. [53] numerically explored the impect of sharp bends and curved corners on rarefied gas flow in the microchannel to obtain thermal 25d hydrothermal behaviors. They reported that a rise in corner radius results in a rise in mass flow rate. Besides that 25 ying curvature as a substitute for sharp turns increase the average shear stress and slip velocity. Aoki et al. [4] studied experimentally bend geometry and confluence in the micromixing. They demonstrated that the mixing feat will be better by combining the confluence and bend channel also the mixing speed is increased b 60 e addition of the confluence angle. Furthermore, the pressure drop produced is equivalent to the channel with or without the bend. Al-Neama et al. [54] conducted both experimentally and numerially investigation on four type configuration design of a rectangular copper microchannel heat sink to obtain the effect of single-phase liquid flow. Its type configuration is straight microchannel, single serpentine, double serpentine and triple serpentine microchannel. They reported the single route serpentine microchannel design presents the most potent heat transfer but also the greatest pressure drop [55].

White et al. [56] conducted numerical studies on the gas flow with varying degrees of rarefaction in a microchannel with 90° bends. That's studies with direct simuzion Monte Carlo. They reported that choosing the right mesh size for the corner area is important so that the shaft and size of the recirculation zone are visible. Rovenskaya [57] conducted the same kind of studies however they used the Navier-Stoks equat 9 for flow rate and Poiseuille number. Nguyen et al. [58] Water flog n a rectangular xerographic microchannel with a ratio of crosssectional area of 0.2, 0.33, and 0.5 was tested experimentally in the ranges of 150 to 3200 Reynolds numbers to obtain minor losses for 90° bends. The reported that the coefficient of minor loses depending on Reynolds number and the area ratio of contraction and expansion in bends.

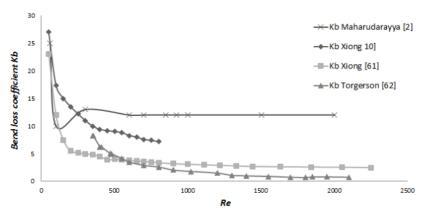


Figure 1. Bend loss coefficient vs Reynolds number

Arun et al. [59] investigated flow properties numerically and empirically of single-phase fluid following through sharp and miter segment 90° bends microchannel sink computational fluid dynamics. They reported that pressure drop of sharp bends higher 307 % than mitered segment bends. Which has been done two-dimensional gas flow simulation by Agrawal et al. [60]. Xiong 21d Chung [10][61] studied flow characteristics and pressure drop in microchannels with hydraulic diameters of 209, 412, and 622 μm of pressure-driven are serpentine rectangular microchannels between 100 and 1700 in the Reynolds number range. They demonstrated that during the Reynolds number transition at 1500-1700, on the Re <100 the vortices not occurred in the bends wall and on the Re > 100 to 1000 the vortices occurred in the constant sharp 9nd size. Torgerson et al. [62] studied experimentally fluid flow in a rectangular xerographic microchannel in the Reynolds number range of 250- 4000 with a 0,45-0,074 channel aspect ratio. They showed that in the critical Re range of 1800 to 2300, the loss coefficient in bend increases when Reynolds number <1200 and decreases significantly when Re above that's. Maharudrayya et al. [2] reported a numerical study on laminar fluid flow in fuel cell microchannel with 1800 bends to investigated pressure drop characteristics and obtained bend loss coefficient. They showed that on the Reynolds number > 1000 bend loss 33 he major part of the total pressure loss.

The bend loss coefficient was shown as a function of Reynolds number in figure 1. Where Maharudrayya et al. [2] and Xiong and Chung [10], using the CFD simulation method while Xiong and Chung [61] and Torgerson et al. [62] using the experimental method. The simulation findings reveal that they do not match the experimental data, whereas Xiong and Chung, [61] and Torgerson et al. [62] experimental results demonstrate the agreement. This study's results may differ due to variances in cross-sectional form and material of microchannel.

## IV. Conclusion

This research is discussing a topic of the characteristics of single-phase fluid flow in microchannels with bends. The possible conclusion be drawn from the given data is that the fluid which flows v 20 a low Reynolds number under 100 does not affect the pressure drop, but on the Reynolds number above that the pressure drop has been increased as the appears of vortices in the outer and inner walls

around the channel bends causes an increase in the additional pressure drop. Whereas a 13 ynolds number above 1000 the bend loss coefficient (Kb) almost remains constant and has fluctuated in the range of  $\pm$  10 %. The other finding shows that the reduction in diameter bend tube can increase the pressure drop. At further research, it is recommended to studies the properties of liquid flow on the microchannel which is influenced by the presence of the variety of bends angles and a wider range of Reynolds numbers, especially to obtain minor loss effect accurately.

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